# CALCULATION OF THE THERMODYNAMIC PROPERTIES OF ALLOYS OF NICKEL AND COBALT

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## CALCULATION OF THE THERMODYNAMIC PROPERTIES OF ALLOYS OF NICKEL AND COBALT

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ABSTRACT. The theory of regular solutions is applied to the problem of determining component activity, thermodynamic quantities and heats of mixing of strongly interacting systems. Formulas are produced for calculation of thermodynamic and thermochemical properties of solutions consisting of components which form large negative and positive asymmetrical deflections from the law of ideal solutions. The intermolecular interaction constants are calculated for many alloys of nickel and cobalt with various elements, which can be used to estimate the concentration dependence of the activity of the components, the mixing heat and the area of existence of two immiscible phases.

Thermodynamic quantities are not only of theoretical interest, since they /35\* allow us to evaluate the nature of the interatomic interaction, but also are of practical value in the determination of gas saturation [1], diffusion processes [2], and furthermore are necessary for the solution of certain technological problems in the production of nonferrous metals [3].

In order to determine the activity of components, the partial and integral thermodynamic quantities and the heats of mixing of strongly interacting systems, the equilibrium between the melt and a chemical compound of practically constant composition near the maximum of the liquidus curve is used; the principles of this method in the framework of the theory of ideal solutions are analyzed in monograph [4]. In the present work, we shall extend the method by applying the theory of regular solutions as well as expressions which take into consideration the asymmetry of the thermodynamic properties.

On the basis of [4], we have the following expression for the points of the maximum

$$\left\langle \left(\frac{d^2 T}{dx_2^2}\right)_{\text{max}} = -\frac{T}{\Delta H(1-x_2)} \left(\frac{d\mu_2}{dx_2}\right)_{\text{max}}, \tag{1}$$

where  $\mu_2$  and  $x_2$  are the chemical potential and atomic fraction of the component, T and  $\Delta H$  are the melting temperature and heat of the chemical

<sup>\*</sup>Numbers in the margin indicate pagination in the foreign text.

compound.

From the theory of regular solutions we have

$$\mu_2 = \mu_2^0 + RT \ln x_2 + (1 - x_2)^2 Q,$$

then after differentiation we find

$$\left(\frac{d^2T}{dx_2^2}\right)_{\text{max}} = -\frac{RT^2}{\Delta Hx_2(1-x_2)} + \frac{2QT}{\Delta H}$$

or

$$Q = \left(\frac{d^2 T}{d x_2^2}\right)_{\text{max}} \frac{\Delta H}{2 T} + \frac{RT}{2x_2(1 - x_2)},$$
 (2)

where Q is the energy of the interchange in the system consisting of components 1 and 2.

Considering an equation from [5]

$$\mu_2 = \mu_2^0 + RT \ln x_2 + (Q_1 + 2Q_2 + 3Q_3) x_1^2 - (2Q_2 + 6Q_3) x_1^3 + 3Q_3 x_1^4$$
(3) /36

after differentiation and substitution in expression (1), we produce

$$\left(\frac{d^2 T}{d x_2^2}\right)_{\text{max}} = -\frac{RT^2}{\Delta H x_2 (1 - x_2)} + \frac{2T (Q_1 + 2Q_2 + 3 Q_3)}{\Delta H} - \frac{6T (Q_2 + 3Q_3) (1 - x_2)}{\Delta H} + \frac{12TQ_3 (1 - x_2)^2}{\Delta H}.$$
(4)

The value of  $\Delta H$  is determined from experimental data or calculated from the additive nature of the melting entropy of the pure components [6]; the numerical values of the heats and temperatures of melting of the components are taken from handbook data [7, 8].

The change in temperature near the maximum is described by a parabola like

$$T = T_0 + a (x_2 - x_2^{\text{m}})^2 + b (x_2 - x_2^{\text{m}})^3,$$
 (5)

where  $x_2^m$  is the concentration of component 2, corresponding to the maximum on the liquidus curve;

a and b are constants defined from experimental data [9].

The results of calculations using equations (2) and (5) are presented together with the initial data in Table 1. The values of the heats and temperatures of melting of nickel and cobalt are taken as 17.7 and 15.7 kj/g·atom, 1455 and 1495° respectively [7].

In nickel melts with Be, Ce, La, Sb, Th, Zr and Co with Si, an asymmetrical deflection is noted, indicating systematic changes in Q for the various compositions. This confirms once again the data of work [5], in which the complex nature of the change in activity with melt composition is noted.

In this case, we must use equations like (3) and (4). Combined solution of three equations (4) for the three compounds allows us to determine the constants  $Q_1$ ,  $Q_2$  and  $Q_3$ . For the system Ni-Ce, this determination gives us  $Q_1 = -187$ ;  $Q_2 = 254$  and  $Q_3 = -156.5$  kj/g·atom. The activity coefficients for 1600° are determined [5] by the expressions

$$\lg f_{\text{Ni}} = -12,3 \, x_{\text{Ce}}^2 + 22,9 \, x_{\text{Ce}}^3 - 13,1 \, x_{\text{Ce}}^4,$$
 
$$\lg f_{\text{Ce}} = -4,15 \, x_{\text{Ni}}^2 + 12,0 \, x_{\text{Ni}}^3 - 13,1 \, x_{\text{Ni}}^4.$$

The results of calculations considering a = fx (Figure 1) indicate a considerable interaction in this system, and if the components are mixed, a considerable quantity of heat is liberated.

In recent years, rare metals are being ever more frequently used for alloying, desulfuration and gas removal, but there is no information at all concerning the mixing heats. However, these data are required for the composition of thermal balances and are the basis for automation of the thermal operation of an aggregate. Calculations of the thermochemical properties can be performed on the assumption that the excess entropy is zero, i.e., by assuming

/ġ·at	t,°C AH'''
1638 20,4	0,50
1472 14,3	0,50
1264 10,7	0,808
1315 15,8	0,167
670 8,7	0,50
485 6,6	0,75
1200 24,2	0,35
1325 16,3	0,167
685 9,6.	0,50
515 7,8	0,75
1145 14,3	0,333
1403 16,7	0,25
1365 16,3	22
730 9,3	0,50
533 7,1	် က
1435 17,2	0,167
1162 19,8	0,286
1153 23,3	0,50
1318 26,8	0,333
992 ( 25,5	0,50
1174 16,3	0,25
1264 18,2	0,40
1545	10

Table	(continued)		0, kj/g·at	-202,6	- 34,6	_ 76,1	-110,8	-152,4	. + 84,1	-236,4	64,7	- 23,1	45,8	- 43,5	-124,5	- 17,8	209,1	-185,2	6,16 —	+4,1	17,7	#P(.)
	equation (2)	•	Equation of liquidus line, t. °C	$t = 1530 - 26000(x_{\rm Th} - x_{\rm Th}^{\rm m})^2 + 85000(x_{\rm Th} - x_{\rm Th}^{\rm m})^3$	$t = 1200 - 8000 (x_{\rm Th} - x_{\rm Th}^{\rm m})^2 + 20000 (x_{\rm Th} - x_{\rm Th}^{\rm m})^3$	$t = 1240 - 10300 (x_{Ti} - x_{Ti}^{m})^{2} + 27500 (x_{Ti} - x_{Ti}^{m})^{3}$	$t = 1310 - 14000(x_{\rm Tl} - x_{\rm Tl}^{\rm m})^2 + 45500(x_{\rm Tl} - x_{\rm Tl}^{\rm m})^3$	$t = 1378 - 18800 (x_{Ti} - x_{Ti}^{m})^{2} + 11300 (x_{Ti} - x_{Ti}^{m})^{3}$	$t = 1380 - 12000 (x_{\text{TI}} - x_{\text{TI}}^{\text{m}})^2$	$t = 1200 - 28000(x_{\rm Zr} - x_{\rm Zr}^{\rm m})^2$	$t = 1740 - 11000(x_{\rm Zr} - x_{\rm Zr}^{\rm m})^2$	$t = 1645 - 5500 (x_{A1} - x_{A1}^{m})^{2} - 19000 (x_{A1} - x_{A1}^{m})^{3}$	$t = 1505 - 10000(x_{\rm Be} - x_{\rm Be}^{\rm m})^2 - 32000(x_{\rm Be} - x_{\rm Be}^{\rm m})^3$	$t = 480 - 7200 (x_{\text{Ce}} - x_{\text{Ce}}^{\text{m}})^2 - 8600 (x_{\text{Ce}} - x_{\text{Ce}}^{\text{m}})^3$	$t = 1200 - 10000(x_{\rm Ge} - x_{\rm Ge}^{\rm m})^2 + 38500(x_{\rm Ge} - x_{\rm Ge}^{\rm m})^3$	$t = 1195 - 2900 (x_{\rm Sb} - x_{\rm Sb}^{\rm m})^2 + 2500 (x_{\rm Sb} - x_{\rm Sb}^{\rm m})^3$	$t = 1332 - 15000(x_{\rm SI} - x_{\rm SI}^{\rm m})^2 + 73000(x_{\rm SI} - x_{\rm SI}^{\rm m})^3$	$t = 1460 - 11000 (x_{\rm SI} - x_{\rm SI}^{\rm m})^2 + 42000 (x_{\rm SI} - x_{\rm SI}^{\rm m})^3$	$t = 1326 - 5300 (x_{\rm SI} - x_{\rm SI}^{\rm m})^2 + 5300 (x_{\rm SI} - x_{\rm SI}^{\rm m})^3$	$t = 1170 - 2100 (x_{\rm Sn} - x_{\rm Sn}^{\rm m})^2 + 5200 (x_{\rm Sn} - x_{\rm Sn}^{\rm m})^3$	$t = 1170 - 5000 (x_{\rm U} - x_{\rm U}^{\rm m})^2 - 19000 (x_{\rm U} - x_{\rm U}^{\rm m})^3$	
	value of Q using		∆H <sup>m</sup> , kj⁄g•at	17,8	13,4	14,9	15,5	16,6	16,6	13,9	20,0	19,2	13,4	6,3	22,4	21,8	25,6	33,7	36,8	15,3	12,9	
	Calculation of value	pund	2° '7	1530	1200	1240	1310	1378	1380	1200	1740	. ≈1645	1505	≈ 480	1200	≈1195	1332	1460	1326	1170	1170	
	Calcuí	Compound	$\kappa_2^{\mathrm{m}}$	0,167	0,50	0,50	0,50	0,25	0,25	0,667	0,25	0,50	0,50	0,75	0,333	0,44	0,333	0,50	0,667	0,35	0,333	
			Formula	Ni <sub>5</sub> Th	NiTh	NiTi	NITI	Ni <sub>3</sub> Ti	NigTi	$NiZr_2$	Ni <sub>3</sub> Zr	CoAl	CoBe	CoCe3	Co <sub>2</sub> Ge	CoSb <sub>0,785</sub>	Co <sub>2</sub> Si	CoSi	CoSi2	CoSn <sub>0,54</sub>	n <sup>z</sup> °o	
			$\Delta H_{\rm o}^{\rm b}$ . kj/g.at	15,7	15,7	18,8	18,8	18,8	18,8	19,2	19,2	10,3	9,6	6,8	33,8	20,1	50,6	50,6	50,6	7,2	12,6	
			System	Ni—Th		Ni—Ti		R		Ni—Zr	R	Co - A1	Co—Be	co—Ce	Co—Ge	Co—Sb	Co—Si		<b>B</b> 7	Co-Sn	Co-U	

$$\Delta H \stackrel{\text{mix}}{=} \Delta G \stackrel{\text{ex}}{,} \tag{6}$$

where  $\Delta G^{\text{ex}}$  is the excess molar Gibbs energy, determined on the basis of the data of [5] by expression

$$\Delta G^{\text{mix}} = Q_1 x_1 x_2 + Q_2 x_1 x_2^2 + Q_3 x_1 x_2^3. \tag{7}$$

The greatest errors introduced by assumption (6) should be observed for melts with high values of Q. For example, in melts of nickel with silicon, the maximum values of the functions are  $\Delta G^{\rm ex} = -46$  kj/g·atom [10], and  $\Delta H^{\rm mix} = -58$  kj/g·atom [10, 11], from which, on the basis of

$$\Delta G^{\mathbf{ex}} = \Delta H^{\mathbf{mix}} T \Delta S^{\mathbf{ex}}$$

at 1600°, the value of  $\Delta S_{ex} = -6.4 \text{ j/g} \cdot \text{atom} \cdot \text{deg}$ . As we can see, the error

introduced by the assumption that  $\Delta S^{ex} = 0$  is 20%, which is greater than the accuracy of the calculations. For weakly interacting systems, the results of calculations from the state diagram (Co-Cu and Ni-Cu melts [5]) are confirmed by direct calorimetric measurements of the mixing heats of nickel and cobalt with copper [12, 13].

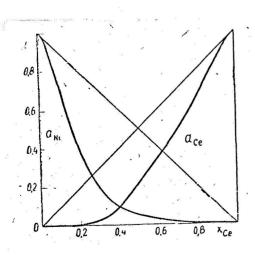


Figure 1. Activity As a Function of Concentration in Ni-Ce Alloys at 1600°

For the system Co-Si, we produce from equation (4)  $Q_1 = -349.5$ ;  $Q_2 = +213.4$  and  $Q_3 = -24.2$  kj/g·atom, from which, on the basis of (6) and (7), we can produce values of  $\Delta H^{mix}$  and  $\Delta G^{ex}$ . Calculations show that the maximum of the functions is located at  $x_{Si} = 0.408$ , which corresponds to the experimental data of [14, 15], but the numerical values of the calculated quantities are somewhat higher than the experimental values.

In order to test other values of Q, we can note that the value of  $Q_{\rm Ni-Ti}$  presented in work [16] almost corresponds with the minimal values for NiTi Ni\_Ti from Table 1. In Ni-Al and Co-Al

alloys, a negative deflection is noted, and the results of the calculations qualitatively correspond with the experimental data [17].

TABLE 2.	CALCULATION OF	VALUES	0F	Q,	AND Q	FROM	EQUATIONS	(8)	AND	(9)	
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	t, °C	Pha Compos	ition "	Q <sub>l</sub> , kj/g•at.	Q <sub>2</sub> , kj/g·at
System		$x_2$	$ x_2 $		
Ag-Ni Ag-Ni* Co-Bi Co-Se Co-Pb* Ni-Tl Ni-Pb Ni-Pb*	1435 1435 1345 1448 1438 1387 1340 1340	0,02 0,0389 0,02 0,034 ≈0,0067 0,025 0,127 0,127	0,97 0,978 0,823 0,31 0,9933 0,96 0,72 0,79	57,7 56,7 53,4 —1,0 72,0 53,4 35,2 35,2	-5,3 -7,5 -30,0 -138,4 - - 5,9 -10,0 - 6,1

For systems with positive deflection, the constants Q, which allow us to determine the thermodynamic and thermochemical properties of the alloys, are determined from the area of immiscibility [9]. The compositions of the phases are determined by the equality of the chemical potentials of the components in both phases (phase numbers marked with primes)

$$\mu_1^{\prime}=\mu_1^{\prime\prime} \text{and} \, \mu_2^{\prime}=\mu_2^{\prime\prime}$$
 ,

from which after substitution of expressions (3) for  $Q_3$  = 0 we produce the two equations

$$RT \ln \frac{x_1'}{x_2''} + \left[ \left( x_2' \right)^2 - \left( x_2'' \right)^2 \right] (Q_1 - Q_2) + \left[ \left( x_2' \right)^3 - \left( x_2'' \right)^3 \right] 2Q_2 = 0, \tag{8}$$

$$RT \ln \frac{x_{2}''}{x_{2}'} + \left[ \left( x_{1}'' \right)^{2} - \left( x_{1}' \right)^{2} \right] (Q_{1} + 2Q_{2}) - \left[ \left( x_{1}'' \right)^{3} - \left( x_{1}' \right)^{3} \right] 2Q_{2} = 0,$$
(9)

joint solution of which allows us to determine  $Q_1$  and  $Q_2$ . Calculations of alloys of cobalt and nickel with various elements [9] are presented in Table 2, where the asterisks mark systems with boundaries of termination of miscibility clarified by the data of [18-21].

Solving equations (8) and (9) for the temperature and fixing of the composition of one phase, we can determine by selection the composition of the second phase for which the values of temperatures from these equations correspond. The critical composition and temperature are determined from the expressions

$$\mathcal{L}_{2}^{\mathbf{r}} = -\frac{Q_{1} - 4Q_{2}}{9Q_{2}} - \sqrt{\left(\frac{Q_{1} - 4Q_{2}}{9Q_{2}}\right)^{2} + \frac{Q_{1} - Q_{2}}{9Q_{2}}} \tag{10}$$

and

$$T_{cr} = \frac{2(Q_1 - Q_2)}{R} x_2^{cr} \left( 1 - x_2^{cr} \right) + \frac{6Q_2}{R} \left( x_2^{cr} \right)^2 \left( 1 - x_2^{cr} \right). \tag{11}$$

An example of the calculation of the area of immiscibility is shown on Figure 2 for the system Ni-Pb.

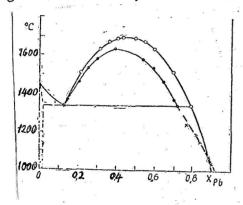


Figure 2. Diagram of State of System Ni-Pb.

x -- Experimental data of [20]; •• -- Calculations using equations (8)-(11)

Using the values of Q which we have found, we can calculate the properties of multi-component systems such as are the real alloys, using the equations produced in works [16, 22].

### Conclusions

- 1. Formulas are produced for calculation of thermodynamic and thermochemical properties of solutions consisting of components which form large negative and positive asymmetrical deflections from the law of ideal solutions.
- 2. The intermolecular interaction constants are calculated for many alloys of nickel and cobalt with various

elements, which can be used to estimate the concentration dependence of the activity of the components, the mixing heat and the area of existence of two immiscible phases.

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